## **TN3TA9**

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Group Art Unit: 1754

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For: DOPED ANIONIC CLAYS

Filing Date: February 7, 2002

Serial No.: 10/072,630

Stamires, Dennis, et al. In re Application of:

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Enclosed herewith is a certified copy of European Patent Application No.

01200831.4, filed March 5, 2001 in connection with the above-identified application.

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Respectfully submitted,

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Attestation

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page, as originally filed. are exact copies of the conformes à la version conformes à la version described on the following page, as originally filed. are exact copies of the

Patentanmeldung Nr.

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Der Präsident des Europäischen Patentamts;

For the President of the European Patent Office

Le Président de l'Office européen des brevets

**B** C van Dijk

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Page 2 de l'attestation Sheet 2 of the certificate

Blatt 2 der Bescheinigung

Am Anmeldetag benannte Vertragataaten:

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NETHERLANDS 6824 BM Arnhem Akzo Nobel N.V.

Demandeur(s): Applicant(s):

State: Pays:

Staat:

Titre de l'invention: Bezeichnung der Erfindung: Title of the invention:

Anmeldung Nr.: Application no.: Demande n°: 4.18800210

Doped antonic clays

Anmeldetag: Date of filing: Date de dépôt:

File no. Numéro de dépôt:

Aktenzeichen:

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DOPED ANIONIC CLAYS

and doped anionic clays prepared by said process. This invention relates to a process for the preparation of doped anionic clays,

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present. Meixnerite is an anionic clay wherein hydroxyl is the predominant anion occurring anionic clay, in which carbonate is the predominant anion present. there are anions and water molecules. Hydrotalcite is an example of a naturally layers built up of specific combinations of metal hydroxides between which Anionic clays have a crystal structure which consists of positively charged

sulphonates such as laurylsulphonate. monocarboxylates such as acetate, dicarboxylates such as oxalate, alkyl  $HVO_4^{2}$ ,  $CIO_4^{1}$ ,  $BO_3^{2}$ , pillaring anions such as  $V_{10}O_{28}^{6}$  and  $Mo_7O_{24}^{6}$ , anions such as NO37, OH, CI7, Br7, I7, SO427, SiO327, CrO427, BO327, MnO47, HGaO327, more particularly carbonate ions, are distributed. The interlayers may contain octahedra alternating with interlayers in which water molecules and anions, In hydrotalcite-like anionic clays the brucite-like main layers are built up of

this specification we refer to these materials as anionic clays, comprising within layered double hydroxide is interchangeably used by those skilled in the art. In is referred to in this specification as an anionic clay. Hydrotalcite-like-and It should be noted that a variety of terms are used to describe the material that

summarised: which the synthesis methods available for anionic clay synthesis have been publications. Two major reviews of anionic clay chemistry were published in The preparation of anionic clays has been described in many prior art that term hydrotalcite-like and layered double hydroxide materials.

Applications," Catalysis Today", 11 (1991) Elsevier Science Publishers B. V. F. Cavani et al "Hydrotalcite-type anionic clays: Preparation, Properties and

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Nostrand Reinhold, N.Y. and microporous solids" (1992), 2, 108, editors: M.I. Occelli, H.E. Robson, Van J P Besse and others "Anionic clays: trends in pillary chemistry, its synthesis Amsterdam.

reformation of the anionic clay structure. whereby the exposure to water of such calcined materials results in the Furthermore, these Mg-Al solid solutions contain a well-known memory effect refer to said disordered MgO-like materials as Mg-Al solid solutions. results upon severe calcination) and from anionic clays. In this specification we product. Said disordered MgO-like product is distinguishable from spinel (which that mild calcination at 500 °C results in the formation of a disordered MgO-like In these reviews the authors state that a characteristic of Mg-Al anionic clays is

metal salts. described for the use of ZnO and CuO in combination with soluble trivalent followed by aging under atmospheric pressure. This method has only been oxide is reacted at atmospheric pressure with a soluble trivalent metal salt, 20 size. The second method is the salt-oxide method in which a divalent metal optionally followed by hydrothermal treatment or aging to increase the crystallite base method) of a soluble divalent metal salt and a soluble trivalent metal salt, conventional method is co-precipitation (in Besse this method is called the salt-Two types of anionic clay preparation are described in these reviews. The most 91

Chemistry Letters (Japan), 843 (1973) For work on anionic clays, reference is further made to the following articles: in the graph of the state of th

Clays and Clay Minerals, 34, 507 (1996) Clays and Clay Minerals, 28, 50 (1980) Clays and Clay Minerals, 23, 369 (1975)

Materials Chemistry and Physics, 14, 569 (1986). 30

In addition there is an extensive amount of patent literature on the use of

anionic clays and processes for their preparation.

Recently, patent applications relating to the production of anionic clays from inexpensive raw materials have been published. These materials include 5 magnesium oxide and aluminium trihydrate.

WO 99/441198 relates to the production of anionic clay from two types of aluminium compounds and a magnesium source. One of the aluminium sources is aluminium trihydrate or a thermally treated form thereof.

WO 99/41196 discloses the preparation of anionic clays with acetate as the charge balancing anion from magnesium acetate, another magnesium source and aluminium trihydrate.

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In WO 99/41195 a continuous process is described for the production of a Mg-Al anionic clay from a Mg source and aluminium trihydrate:

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WO 99/41197 discloses the production of an anionic clay-containing composition comprising a Mg-Al anionic clay and unreacted aluminium trihydrate or a thermally treated form thereof

Several patents in the name of Alcoa describe the synthesis of hydrotalcites, in a batchie. anionic clays, but of magnesium oxide and a transition alumina, in a batchwise manner and under non-hydrothermal conditions: US 5,728,364 US 5,728,365, US 5,728,366, US 5,730,951, US 5,776,424, US 5,728,286. The comparative Examples 1-3 presented in all these patents indicate that upon using aluminium trihydrate as aluminium source, anionic clays are not formed.

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There are many applications of anionic clays. These include but are not restricted to: catalysts, adsorbents, drilling muds, catalyst supports and carriers, extenders and applications in the medical field. In particular Van Broekhoven

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(US 4,956,581 and US 4,952,382) has described their use in SO<sub>x</sub> abatement chemistry.

For several applications the presence of additives, both metals and non-metals, within the anionic clay is desirable. These additives are used to alter or enhance certain properties of the anionic clay. For instance, Ce and V are added to the anionic clay to obtain material suitable for SOx removal in FCC. In general, these additives are deposited on the anionic clay by impregnation. With impregnation, however, it is often difficult to obtain a homogeneous dispersion of the additive within the anionic clay or it is difficult to deposit

enough additive on the anionic clay to obtain the desired properties.

Some patent publications indicate that the additives may be added to the reaction mixture during preparation of the anionic clay. However, when additives are added to the reaction mixture, when anionic clays are made by coprecipitation it is possible that the pH required to precipitate for example the precipitation it is possible that the pH required to precipitate for example the precipitation it is possible that the pH required to precipitate for example the precipitation it is possible that the pH required to precipitate for example the additive. In extreme situations the additive may be precipitated in advance of the magnesium and aluminium sources or may not be sufficiently precipitated of the magnesium in solution.

This invention relates to a process for preparing doped anionic clays, wherein anionic clay can be prepared containing controlled amounts of additive chereinafter referred to as dopant). Further, the process allows controlled 25 (hereinafter referred to as dopant).

dispersion of the dopant within the anionic clay.

The process according to the invention pertains to the preparation of doped anionic clay wherein a trivalent metal source is reacted with a divalent metal source, at least one of the metal sources being either doped boehmite or a doped magnesium source, i.e. doped brucite or doped MgO, to obtain a doped doped magnesium source, i.e. doped brucite or doped MgO, to obtain a doped

anionic clay.

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It was found that when using a doped starting material such as doped boehmite and/or doped magnesium source, the amount of dopant can be dispersed homogeneously and enough additive can be deposited on the anionic clay. It was found further that the dopant present either in the magnesium source and/or boehmite does not interfere with the formation of the anionic clay.

Upon being heated anionic clays generally form solid solutions, and at higher temperatures spinels. When used as a catalyst, an adsorbent (for instance a  $SO_x$  adsorbent for catalytic cracking reactions), or a catalyst support, the anionic clay according to the invention is usually heated during preparation and is thus in the solid solution form. During use in a FCC unit, the catalyst or adsorbent is converted from an anionic clay into a solid solution.

Therefore, the present invention is also directed to a process wherein a doped anionic clay prepared by the process according to the invention, is heat-treated at a temperature between 300° and 1200°C to form a doped solid solution and/or spinel.

Doped boehmite

As mentioned above, in the process according to the invention a doped boehmite and/or a doped magnesium source is used as starting material for the doped anionic clay. The doped boehmite used in the process according to the invention can be prepared in several ways. In general, a boehmite precursor and an additive are converted to a boehmite containing the additive in a homogeneously dispersed state. Suitable additives are compounds containing elements selected from the group of alkaline earth metals (for instance Ca and Ba), alkaline metals, transition metals (for example Mn, Fe, Ti, Zr, Cu, Ni, Zn, Mo, W, V, Sn), actinides, rare earth metals such as La, Ce, Nd, noble metals

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such as Pt and Pd, silicon, gallium, boron, titanium, and phosphorus.

washing, as anions undesirable for catalytic purposes are not present. because the resulting boehmites with additive can be dried directly, without any etcetera. The use of compounds with heat-decomposable anions is preferred, S chlorides, formates, acetates, oxalates, alkoxides, carbonates, vanadates, Suitable compounds containing the desired elements are nitrates, sulphates,

NOTE: THE CONTRACT OF STREET described below: Examples of suitable preparation processes for the doped boehmites are December 2014 of the Company of the

Process 1

aging step. A transfer of the manager of the second of can be incorporated during the hydrolysis step or added at the end before the in the presence of a compound containing the desired additive(s). The additive The boehmite can be prepared by hydrolysing and aging an aluminium alkoxide

A Process 2 who was the state of the seasons and the seasons of th 

added while the hydrolysis and precipitation are going on or at the end in the chloride, sodium aluminate, and mixtures thereof. The additive(s) may be suitable aluminium salts are aluminium sulphate, aluminium nitrate, aluminium soluble aluminium salts and aged to form a doped boehmite. Examples of The boehmite can be prepared by hydrolysis and precipitation as hydroxides of A control of the control of the See Seet of the control of the control

医乳腺 植物的种类形式 医多克氏管 医皮肤 aging step.

Process 3

thermally treated form of aluminium trihydrate and additive(s) at temperatures The boehmite can also be prepared by aging an aqueous slurry containing a

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temperature between 80 and 150°C. Thermally treated forms of aluminium trihydrate are calcined aluminium trihydrate and flash calcined aluminium trihydrate and flash calcined aluminium trihydrate and flash calcined aluminium trihydrate (CP ® alumina). This preparation method has the advantage that no ions are introduced into the boehmite apart from any ions present in the additive compound. That means that with the appropriate choice of additive compounds washing steps can be reduced or avoided altogether. For instance, when decomposable anions (such as catbonates, nitrates, and formates and oxalates) are used, the doped boehmite can be dried directly, as cations undesirable for catalytic purposes are not present.

Process 4

The doped boehmite can also be prepared by aging an aqueous slurry containing amorphous alumina gel and additive(s) at temperatures ranging from 60° to 250°C, preferably at a temperature between 80° and 150°C, to form boehmites. Like process 3 mentioned above, this preparation method also has the advantage that no ions are introduced into the boehmite apart from the ions of the additive compound. This means that with the appropriate choice of additive compounds washing steps can be reduced or avoided altogether.

Process 5

Doped boehmites to be used according to the invention can also be prepared by aging a relatively amorphous boehmite by thermal or hydrothermal treatment in the presence of compounds of the desired additive to form a boehmite containing additive in a homogeneously dispersed state. More in particular, quasi-crystalline boehmites can be aged in the presence of additive. If this aging is performed under hydrothermal conditions, doped micro-crystalline boehmite will be obtained; if this aging is conducted thermally doped quasi-crystalline boehmite will be obtained.

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No ions other than the ions of the additive compound are introduced into the boehmite with this process.

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Process 6

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Doped Boehmites can also be prepared by aging aluminium trihydrates such as gibbsite, BOC, and bayerite by hydrothermal treatment, with the aid of suitable boehmite seeds in the presence of compounds of the desired additives.

Suitable seeds are the known seeds to make microcrystalline boehmite such as commercially available boehmite (Catapal®, Condea P3®, Versal, P-200®, etcetera), amorphous seeds, milled boehmite seeds, boehmite prepared from sodium aluminate solutions, etcetera. Additionally, the seeds may have been described above can suitably be used as a seed. Like processes described above can suitably be used as a seed. Like processes 3, 4, and 5 no described above can suitably be used as a seed. Like processes 3, 4, and 5 no ions other than the ions of the additive (and the optional additives present in the seed) are introduced into the boehmite.

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Combinations of doped boehmites or combinations of doped boehmite and another trivalent metal source can also be used. Preferably the doped boehmite is added to the reactor in the form of an aqueous suspension or slurry. As mentioned above, in the process according to our invention trivalent metal sources beside (or other than) doped boehmite may be added to the aqueous suspension such as oxides and hydroxides of aluminium, (e.g. sols, flash calcined alumins, gels, non-doped boehmite) aluminium salts such as aluminium nitrate, aluminium chloride, aluminium chlorohydrate and sodium aluminate, as well as sources of gallium, indium, iron, chromium, vanadium, cobalt, manganese sources are the respective oxides, hydroxides, oxalates, carbonates, nitrates, chlorides, chlorohydrates, and alkoxides. Also mixtures of carbonates, nitrates, chlorides, chlorohydrates, and alkoxides. Also mixtures of the above-mentioned trivalent metal sources can be used.

the above-mentioned trivalent metal sources can be used. By using a combination of doped boehmite and non-doped aluminium sources

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improves the nickel encapsulation capacity of the anionic clay. instance, alumina provides acid sites for catalytic cracking and boehmite provide different types of desirable functionalities for the anionic clay. For alumina improves the binding properties of the anionic clay and may also to convert all of the trivalent metal source into doped anionic clay. Excess combinations thereof, all optionally in the presence of seeds. It is not necessary treatment with acid or base, thermal and/or hydrothermal treatment, or to the addition to the reaction mixture. Said pre-treatment may involve The doped boehmite and other trivalent metal sources may be pre-treated prior the amount of dopant present in the final anionic clay can be controlled.

Doped magnesium source

be prepared, with the dopants being present in a homogeneously dispersed to obtain the doped magnesium source. In this way doped brucite or MgO can precursor thereof in an aqueous suspension and thermally treating said mixture by adding an additive such as the ones described-above to brucite, MgO or a Doped magnesium source, i.e. doped brucite or doped MgO, can be prepared

cobalt, manganese, calcium, barium. Suitable zinc, nickel, copper, iron, cobalt, the aqueous suspension such as metal sources of zinc, nickel, copper, iron, 30 sources beside (or other than) the doped magnesium source may be added to mentioned above, in the process according to our invention divalent metal added to the reactor in the form of an aqueous suspension or slurry. As metal source can also be used. Preferably the doped magnesium source is sources or combinations of a doped magnesium source and another divalent 52 clays such as dolomite, saponite, sepiolite. Combinations of doped magnesium bicarbonate, magnesium nitrate, magnesium chloride, magnesium-containing acetate, magnesium carbonate, magnesium hydroxy carbonate, magnesium salts such as magnesium acetate, magnesium formate, magnesium hydroxy Suitable brucite or MgO precursors are Mg(OH)2, hydromagnesite, magnesium THE SOLOR MAP TOO THE WAY SHOW THE TELEST

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thereof, optionally in the presence of seeds. and/or a hydrothermal treatment, an acid or base treatment, or combinations addition to the reaction mixture. Said pre-treatment may comprise a thermal sources can be used. The divalent metal source may be pre-treated prior to the nitrates, chlorides. Also mixtures of the above-mentioned divalent metal manganese, calcium, barium sources are oxides, hydroxides, carbonates,

magnesium source the amount of dopant in the anionic clay can be controlled. By using of a combination of doped magnesium source and non-doped

scid streams of gases ordiquids are well and are properly and streams of gases ordiquids. sites which render the anionic clay suitable for removing or neutralising strong as for instance metal trap capacity. The presence of magnesia provides basic alumina-magnesia in the anicnic clay may provide desirable functionalities such 15 be referred to in the description as magnesia. The presence of magnesia or the sake of clarity, this excess of magnesium compounds in the anionic clay will brucite, magnesia or alumina-magnesia, doped or not, as the case may be. For another magnesium source will usually be present in the final product as clay. For instance, any excess magnesium, either doped brucite, doped MgO or It is not necessary to convert all of the divalent metal source into doped anionic

Doped boehmite and doped magnesium source

compounds can be same or different. 52 source are used in the process, the additive (dopant) in these doped In the embodiment in which both doped boehmite and doped magnesium

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Conditions

to obtain a doped anionic clay. Within the context of this invention a reactor is metal sources are added to a reactor and heat-treated in aqueous suspension The doped starting material(s) and optionally additional divalent and/or trivalent

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considered to be any confined zone in which the reaction between the trivalent metal source and divalent source takes place. The reactor may be equipped with stirrers, baffles, etceters to ensure homogeneous mixing of the reactants. The reaction can take place with or without stirring and at temperatures between 50° and 100°C at atmospheric pressure and at higher temperatures (up to 400 °C) at increased pressure, i.e under hydrothermal conditions. The reactor may be heated by any heating source such as a furnace, microwave, infrared sources, heating jackets (either electrical or with a heating fluid), lamps, infrared sources, heating jackets (either electrical or with a heating fluid), lamps,

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The process according to the invention may be conducted batch-wise or in a continuous mode, optionally in a continuous multi-step operation. The process may also be conducted partly batch-wise and partly continuously.

The final anionic clay may conveniently be obtained by drying the resulting mixture.

If desired, organic or inorganic acids and bases, for example for control of the pH, may be fed to the reactor or added to either the divalent metal source or the trivalent metal source before they are fed to the reactor. An example of a preferred pH modifier is an ammonium base, because upon drying no

deleterious cations remain in the anionic clay.

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The product formed may optionally be calcined at temperatures between 300° and 1200°C, preferably between 300° and 800°C and most preferred between 300° and 600°C. This calcination is conducted for 15 minutes to 24 hours, preferably 1-12 hours and most preferred 2-6 hours. By this treatment the anionic clay will be transformed into a solid solution and/or spinel. Solid solutions posses the well known memory effect, which means that they can be transformed back into anionic clays upon rehydration. This rehydration can be performed by contacting the solid solution with water for 1-24 hours at 65°-85°C. Preferably, the slurry is stirred and has a solids content ranging from about 10 to 50 wt%. During this treatment additives can be added.

If desired, the doped anionic clay prepared by the process according to the invention may be subjected to ion-exchange. Upon ion-exchange the interlayer charge-balancing anions are replaced with other anions. Said other anions are the ones commonly present in anionic clays and include pillaring anions are the ones commonly present in anionic clays and include pillaring anions are given in as V<sub>2</sub>O<sub>7</sub><sup>+</sup>, HV<sub>2</sub>O<sub>12</sub><sup>+</sup>, V<sub>3</sub>O<sub>9</sub><sup>-</sup>, V<sub>4</sub>O<sub>26</sub><sup>-</sup>, Mo<sub>7</sub>O<sub>24</sub><sup>-</sup>, PW<sub>12</sub>O<sub>40</sub><sup>-</sup>, B(OH)<sub>4</sub><sup>-</sup>, [B<sub>3</sub>O<sub>3</sub>(OH)<sub>4</sub>], [B<sub>3</sub>O<sub>3</sub>(OH)<sub>4</sub>], [B<sub>3</sub>O<sub>3</sub>(OH)<sub>5</sub>], HBO<sub>4</sub><sup>2</sup>, HGaO<sub>2</sub><sup>2</sup>, CrO<sub>4</sub><sup>2</sup>, Reggin-ions, formates, as V<sub>2</sub>O<sub>7</sub><sup>+</sup>, HV<sub>2</sub>O<sub>12</sub><sup>+</sup>, V<sub>3</sub>O<sub>9</sub><sup>2</sup>, V<sub>4</sub>O<sub>26</sub><sup>2</sup>, Mo<sub>7</sub>O<sub>24</sub><sup>2</sup>, PW<sub>12</sub>O<sub>40</sub><sup>2</sup>, Reggin-ions, formates, as a V<sub>2</sub>O<sub>7</sub><sup>+</sup>, HV<sub>2</sub>O<sub>12</sub><sup>-</sup>, V<sub>3</sub>O<sub>9</sub><sup>2</sup>, Mo<sub>7</sub>O<sub>26</sub><sup>2</sup>, HGaO<sub>3</sub><sup>2</sup>, CrO<sub>4</sub><sup>2</sup>, Reggin-ions, formates, as a V<sub>2</sub>O<sub>7</sub><sup>2</sup>, HV<sub>2</sub>O<sub>12</sub><sup>2</sup>, V<sub>3</sub>O<sub>9</sub><sup>2</sup>, Mo<sub>7</sub>O<sub>26</sub><sup>2</sup>, HBO<sub>4</sub><sup>2</sup>, HBO

The process of the invention provides wide flexibility in preparing products with a wide range of divalent to trivalent metal molar ratios. This ratio can vary from 2 to 10, preferably from 1 to 6, more preferred from 2 to 4, and especially preferred close to 3.

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In addition to the additives already incorporated into the anionic clay by using the doped boehmite or doped magnesium source, it may be desirable to add additional additives, both metal compounds and non-metal compounds, such as rare earth metals, Si, P, B, group VI, group VIII, alkaline earth (for instance

Ca and Ba) and/or transition metals (for example Mn, Fe, Ti, Zr, Cu, Ni, Zn, Mo, Sn, V, W), to the anionic clay. Said additives can be deposited on the doped anionic clay according to the invention or they can be added either to the divalent metal source or the trivalent metal source which are added to the reactor or added to the reactor separately. Suitable sources of metal compounds or non-metal compounds are oxides, halides or any other salt such as chlorides, nitrates etcetera.

If an excess of trivalent compound is used a composition is obtained which contains doped anionic clay and also trivalent metal compound usually in the form of an oxide or hydroxide.

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On the other hand, divalent metal sources may be used in excess to obtain a composition containing doped anionic clay and a divalent metal compound,

usually in the form of an oxide or hydroxide:

It is even possible to prepare compositions containing anionic clay, trivalent
metal compound and a divalent metal compound with the process according to

the invention by controlling the process conditions: In said compositions the doped anionic clay, divalent metal compound are intimately mixed, rather than present as separate phases such as in physically mixed mixtures of doped anionic clay, divalent

metal compound and/or trivalent metal compound.

These compositions appear to be highly suitable for use as an additive or as a matrix for catalysts for hydrocarbon conversion. Moreover, these compositions appears especially suitable for sulphur removal from the gasoline and diesel fraction in FCC, SO<sub>x</sub> and NO<sub>x</sub> removal in FCC, and as a metal trap.

The resulting doped anionic clays may optionally be shaped to form shaped bodies. If composites containing doped anionic clay and (doped) boehmite are formed, this boehmite can serve as a binder and create porosity in the shaped

30 bodies.

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catalyst components or precursors thereof may be added prior to the shaping zeolite, ZSM-5, beta-zeolite, ST-5 etcetera). Typically, such conventional etcetera), molecular sieve material (e.g. zeolite Y USY zeolite, ion- exchanged such as kaolin, titanium oxide, zirconia, alumina, silica, silica-alumina, bentonite conventional catalyst components such as matrix or filler materials (e.g. clay The doped anionic clay-containing bodies may also be prepared to contain

methods such as extrusion additives may be added to the precursor mixture suitable for shaping. Various additives commonly used in the various shaping change the pH of the precursor mixture to make the slurry gellable and thus liquid used in the slurry and/or add an additional or another liquid, and/or shaping step to be conducted. It might be advisable to partially remove the of liquid present in the slurry used for shaping should be adapted to the specific used in the catalyst and absorbent fields or combinations thereof. The amount 10 combined with kneading), beading, or any other conventional shaping method Suitable shaping methods include spray-drying, pelletising, extrusion (optionally

composition. 20 The doped anionic clay can suitably be used as a component of a catalyst وي ويصف في برود يا وي الله وي الطعميان إليقة في يا ياني أنان بي . . . هو يا هي أن يا يا يا يا يا يا ي

The present invention is illustrated by the following examples. 

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**EXAMPLES** 

Example 1

A suspension of Condea P-3@ alumina in a Zn(NO<sub>3</sub>)<sub>2</sub> solution was homogenised by high shear mixing for 15 minutes. The mixture was aged at 85°C for 24 hours. This resulted in a Zn<sup>2+</sup> doped boehmite containing around 10 wt% ZnO.

To the doped boehmite-containing slurry a MgO-containing slurry with a pH of 7.42 and a temperature of 44°C was added in an amount sufficient to obtain a Mg/Al molar ratio of 2.3. Subsequently, the mixture was aged at 85°C for 24 hours. The slurry had a solids content of approximately 25 wt% and a pH of 8.92. The final product was dried at 100°C. Powder X-ray diffraction (PXRD) indicated the formation of anionic clay.

Example 2

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A suspension of Condea P-3@ alumina in a Zn(NO<sub>3</sub>)<sub>2</sub> solution was homogenised by high shear mixing for 15 minutes. The mixture was aged at 20 S°C for 24 hours: This resulted in a Zn<sup>2+</sup> doped boehmite containing around 10

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To the doped boehmite-containing slurry a MgO-containing slurry with a pH of 7.42 and a temperature of 44°C was added in an amount sufficient to obtain a Mg/Al molar ratio of 2.3. Subsequently, the mixture was aged hydrothermally at 165°C and autogenous pressure for 2 hours. The slurry had a solids content of approximately 25 wt% and a pH of 8.92. The final product was dried at 100°C. PXRD indicated the formation of anionic clay.

Example 3

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A suspension of Condea P-3@ alumina in a  $Zn(NO_3)_2$  solution was

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homogenised by high shear mixing for 15 minutes. The mixture was aged at  $85^{\circ}$ C for 24 hours. This resulted in a  $Zn^{2+}$  doped boehmite containing around 10

To the doped boehmite-containing slurry a MgO-containing slurry with a pH of To the doped boehmite-containing slurry a MgO-containing slurry with a pH of A4°C was added in an amount sufficient to obtain a Mg/AI molar ratio of 2.3. Following addition of NaCH/Na<sub>2</sub>CO<sub>3</sub> (1M final concentration), the mixture was aged at 85°C for 24 hours. The initial pH of the slurry was 10. The product was filtered, washed with water and dried at 100°C. PXRD indicated the formation of anionic clay.

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Example 4

La $_2O_3$ -doped quasi-crystalline boehmite was prepared by co-precipitating aluminium sulphate and sodium aluminate to a final pH of 10, at 85°C and in the presence of La(NO $_3$ ) $_3$ . The precipitate was aged at 80°C for 24 hours and subsequently dried at 90°C overnight. The doped boehmite contained 10 wt%

 $La_2O_3$ . MgO and  $Na_2CO_3$  (final concentration 1M) were added to the doped boehmite-containing slurry. The Mg/Al ratio in the slurry was 2.3. The resulting slurry was 2.3. The resulting slurry as aged at 80°C for 12 hours. The product was filtered and dried overnight at

100°C. PXRD indicated the formation of anionic clay.

Example 5

CeO<sub>2</sub>-doped boehmite was prepared by suspending Condea P-3® alumina in a  $(NH_4)_2$ Ce $(NO_3)_6$  solution with a pH of 7.42 and a temperature of 44°C with high shear mixing for 15 minutes. The suspension was treated at 85°C for 24 hours. The product was not dried. The resulting doped boehmite containing around 10  $\times$  0.00  $\times$ 

MgO was added to the slurry. The resulting slurry had a pH of 8.92, a solids content of about 25 wt% and a temperature of 52°C. The Mg/Al ratio in the

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dried overnight at 100°C. PXRD indicated the formation of anionic clay. slurry was 2.3. The slurry was aged at 85°C for 24 hours. The product was

Example 6

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The product was not dried. The resulting doped boehmite containing around 10 shear mixing for 15 minutes. The suspension was aged at 85°C for 24 hours.  $(NH_4)_s$ Ce $(NO_5)_e$  solution with a pH of 7.42 and a temperature of 44°C with high  ${\rm CeO_2\text{-}doped}$  boehmite was prepared by suspending Condea P-3® alumina in a

The first of the f indicated the formation of anionic clay. pressure for 4 hours. The product was dried overnight at 100°C, PXRD slurry was 2.3. The slurry was aged hydrothemally at 165°C at autogenous content of about 25 wt% and a temperature of 52°C. The Mg/AI ratio in the MgO was added to the slurry. The resulting slurry had a pH of 8.92, a solids wt% CeOs. 10

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- obtain a doped anionic clay. sources being either doped boehmite, doped MgO or doped brucite, to S source is reacted with a divalent metal source, at least one of the metal Process for the preparation of doped anionic clay wherein a trivalent metal
- divalent metal source. Process according to claim 1, wherein doped boehmite is reacted with a .2
- trivalent metal source. Process according to claim 1 or 2, wherein doped brucite is reacted with a Ξ. 10
- reacted with a trivalent metal source. 91 Process according to any one of the claims 1-3, wherein doped MgO is ·Þ
- another trivalent metal source is present in the reaction mixture. Process according to claim 2 wherein in addition to the doped boehmite
- another divalent metal source is present in the reaction mixture. Process according to claim 3 wherein in addition to the doped brucite 20
- another divalent metal source is present in the reaction mixture. Process according to claim 4 wherein in addition to the doped MgO
- conditions. source and the divalent metal source are reacted under hydrothermal Process according to any one of claims 1-7 wherein the trivalent metal .8 52
- the doped MgO and/or the doped brucite contain a rare earth metal Process according to any one of claims 1-8 wherein the doped boehmite, 6 30

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- 10. Process according to any one of the previous claims, wherein the doped boehmite, the doped MgO and/or the doped brucite is added in excess to obtain a compositions comprising anionic clay and doped boehmite, doped MgO and/or doped brucite.
- Process for the preparation of a doped Mg-Al solid solution and/or spinel, wherein an anionic clay obtained by any one of the processes according to any one of the previous claims is subjected to a heat-treatment at a temperature between 300° and 1200°C.
- 12. Process for the preparation of doped anionic clay, wherein the Mg-Al solid solution obtained by the process of claim 11 is rehydrated to form a doped anionic clay.
- 13. Doped anionic clay obtainable the process according to any one of claims 1-10 or 12.
- 20 14. Shaped body comprising doped anionic clay according to claim 13.
- 15. Catalyst composition containing doped anionic clay according to claim-13.
- .55 claim 13.

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The present invention is directed to a process for the preparation of a doped anionic clay. In said process a trivalent metal source is reacted with a divalent of metal source, at least one of the metal sources being either doped boehmite, doped MgO or doped brucite, to obtain a doped anionic clay.

Suitable dopants are compounds containing elements selected from the group

of alkaline earth metals ( for instance Ca and Ba), alkaline metals, transition metals (for example Mn, Fe, Ti, Zr, Cu, Ni, Zn, Mo, W, V, Sn), actinides, rare earth metals such as La, Ce, Nd, noble metals such as Pt and Pd, silicon, gallium, boron, titanium, and phosphorus.

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